WHAT IS CLAIMED IS:

1. A process for producing stable lubricant bright stock comprising the steps of:

a) providing a petroleum residuum-derived stream having a sulfur content of less than 1% and a nitrogen content of less than 0.5%;

b) separating the residuum-derived stream at a distillation cut point in the range of 1150°F to 1300°F, into a heavy fraction and at least one light fraction;

c) hydrocracking the at least one light fraction under lube hydrocracking in a lube hydrocracking zone in the presence of a hydrocracking catalyst and hydrogen under conditions to reduce the concentration of sulfur and nitrogen to suitable levels for hydroisomerization dewaxing; and

d) dewaxing at least a portion of the hydrocracked stream in an hydroisomerization zone in the presence of a hydroisomerization catalyst and hydrogen under hydroisomerization conditions to produce a lubricant bright stock.

2. The process of Claim 1, wherein the petroleum residuum-derived stream is a hydrocracked deasphalted oil.

3. The process of Claim 1, wherein the petroleum residuum-derived stream is a hydrocracked residuum.

4. The process of Claim 1, wherein the petroleum residuum-derived stream has a concentration of sulfur of less than 0.5% and a concentration of nitrogen of less than 0.2%.

5. The process of Claim 1, further comprising stabilizing the lubricant bright stock in a hydrofinishing zone in the presence of a hydrofinishing catalyst and hydrogen under hydrofinishing conditions.

6. The process of Claim 5, further comprising contacting the stabilized lubricant bright stock with clay in a clay treatment zone.

7. The process of Claim 1, wherein the bright stock has a viscosity, measured at 100°C, of greater than 15 cSt and viscosity index of greater than 80.

8. The process of Claim 7, wherein the bright stock has a viscosity index of greater than 90.

9. The process of Claim 1, wherein the bright stock has a viscosity in the range of 20 and 60 cSt, measured at 100°C.

10. The process according to Claim 1, wherein the hydroisomerization catalyst is selected from the group consisting of SAPO-11, SAPO-31, SAPO-41, SM-3, ZSM-22, ZSM-23, ZSM-35, ZSM-48, ZSM-57, SSZ-32, offretite, ferrierite and combinations thereof.

11. The process according to Claim 10, wherein the hydroisomerization catalyst is selected from the group consisting of SAPO-11, SAPO-31, SM-3, SSZ-32, and ZSM-23.

12. The process according to Claim 11, wherein the hydroisomerization catalyst is selected from the group consisting of SAPO-11, SM-3, SSZ-32, and ZSM-23.

13. The process according to Claim 1, wherein the hydroisomerization catalyst has a metal hydrogenation component.

14. The process according to Claim 13, wherein the metal hydrogenation component is platinum, palladium, or a mixture thereof.

15. The process according to Claim 10 wherein the metal hydrogenation component is platinum.

16. The process according to Claim 1, wherein the suitable levels for hydroisomerization dewaxing include a concentration of nitrogen of less than 50 ppm and a concentration of sulfur of less than 100 ppm.

17. The process according to Claim 1, wherein the suitable levels for hydroisomerization dewaxing include a concentration of nitrogen of less than 30 ppm and a concentration of sulfur of less than 50 ppm.

18. The process according to Claim 1, wherein the suitable levels for hydroisomerization dewaxing include a concentration of nitrogen of less than 10 ppm and a concentration of sulfur of less than 20 ppm.